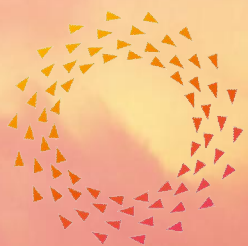


DIRECT AIR CAPTURE - THE EFFECT OF HUMIDITY ON ADSORBENT PERFORMANCE



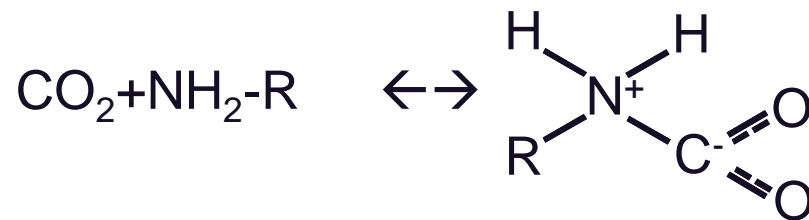
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Jere Elfving, VTT

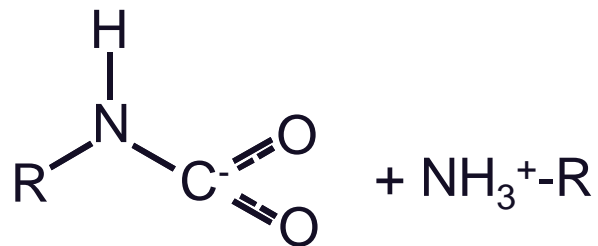
Neo-Carbon Energy 7th Researcher's seminar
24.-25.1.2017 Lappeenranta

Introduction

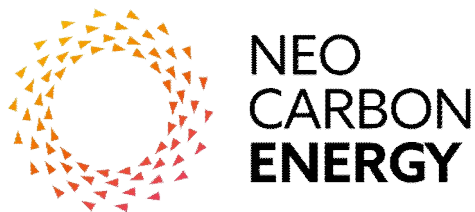
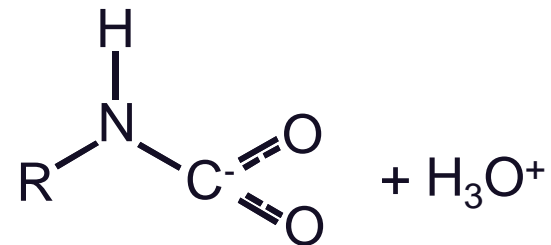
For primary & secondary amines



Dry conditions



Humid conditions

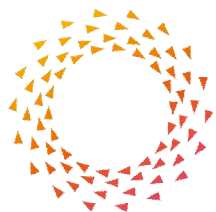


- In dry conditions: $\text{CO}_2/\text{N}=1/2$
- In humid conditions: $\text{CO}_2/\text{N}=1/1$
- Higher capacity in humid conditions

The effect of humidity

- Results differ, for example:
 - 2.25→2.58 mmol/g (15% increase)
 - 80% RH, 25°C (MC with PEI)*
 - 1.11→2.13 mmol/g (92% increase)
 - 91% RH, 23°C (NFC with aminosilane)**
 - 0.5→2.25 (350% increase)***
 - 20→80% RH, 25°C (NFC with PEI)
- In some cases, even negative effect
 - Less capacity
 - Degradation of support or amine
 - Especially in zeolites and MOFs

→ Important to determine sorbent-specifically



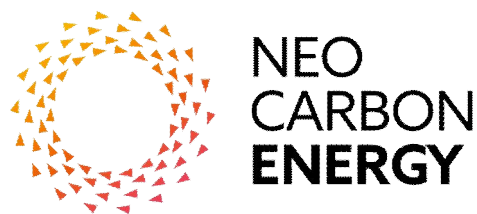
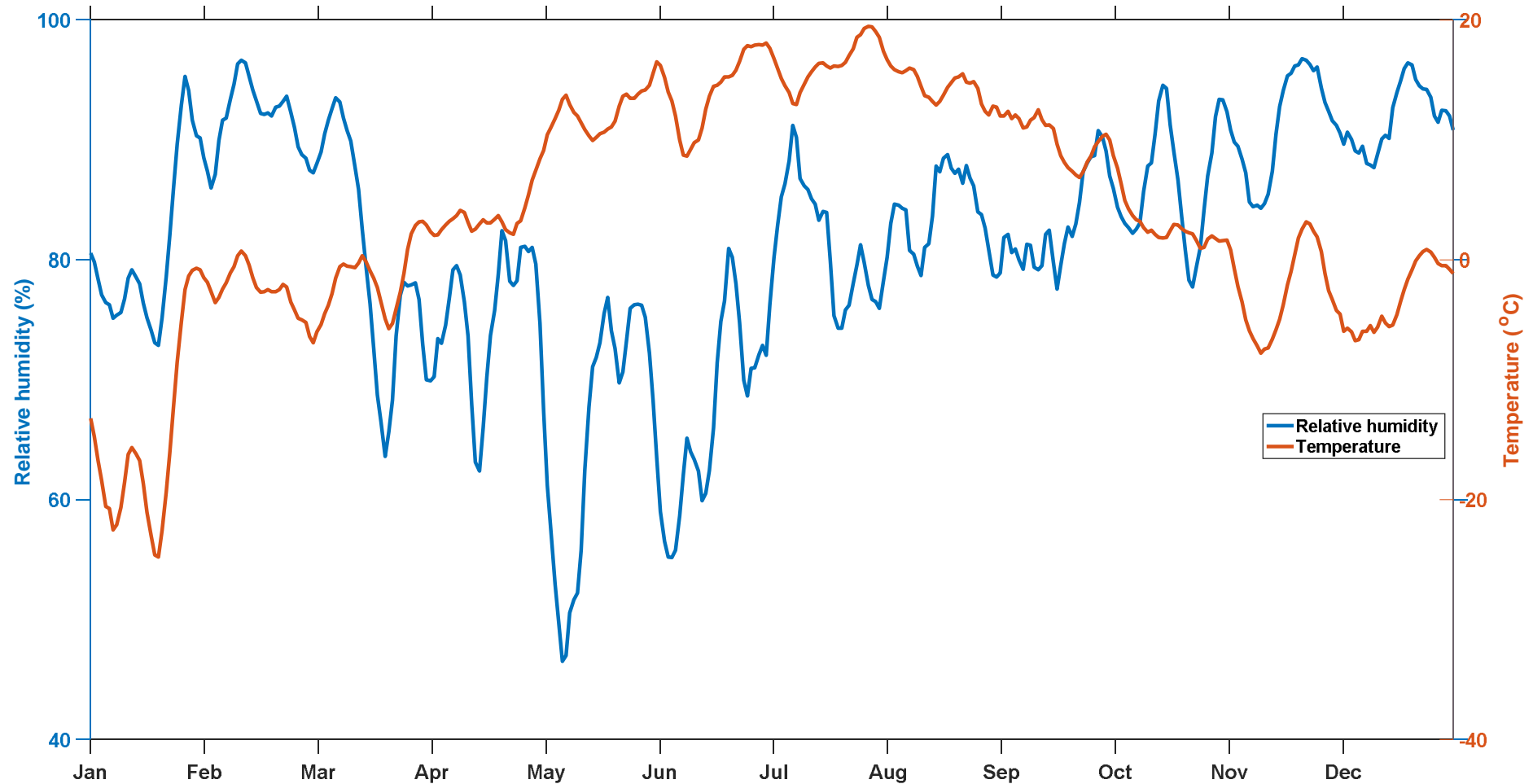
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*J. Wang et al., Direct capture of low-concentration CO₂ on mesoporous carbon-supported solid amine adsorbents at ambient temperature, *Ind. Eng. Chem. Res.* 54 (2015) 5319–5327.

**C. Gebald et al., Single-Component and Binary CO₂ and H₂O Adsorption of Amine-Functionalized Cellulose, *Environ. Sci. Technol.* 48 (2014) 2497-2504.

***Sehaqui et al., Fast and reversible direct CO₂ capture from air onto all-polymer nanofibrillated cellulose—polyethylenimine foams, *Environ. Sci. Technol.*, 49 (2015) 3167–3174

Averaged temperature & relative humidity

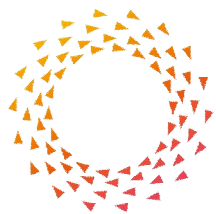


Averages from end of July:
 $T=19.5^{\circ}\text{C}$, $\text{RH}=78\%$
 $\rightarrow 1.77 \text{ vol-\%}$

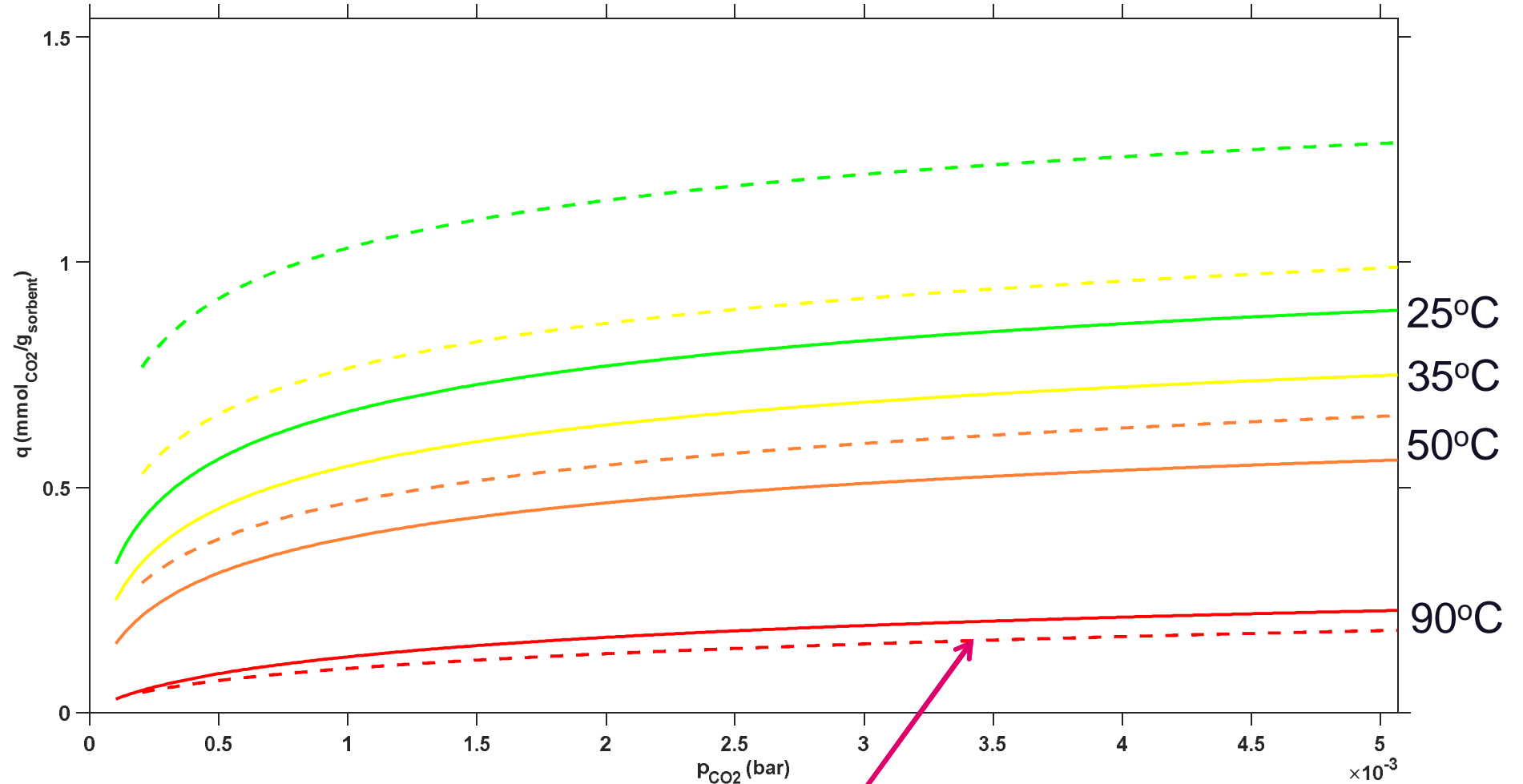
Source of data: FMI open data, JKL Airport real time observations, 1.1.2016-31.12.2016

Methods

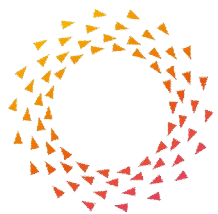
- Laboratory-scale fixed-bed adsorption
 - 0.5 grams of resin
 - Flow rate 1l/min
 - FTIR measurement of gas species
→capacities by integration
- 2 vol-% H₂O was used
 - A reasonable value in summer conditions
 - 63% relative humidity at 25°C
- 6 partial pressures of CO₂, 4 temperatures
- The results here calculated for resin mass as received
 - 9-10% higher for completely dry and CO₂ free sorbent
- Temperature-dependent Toth model used for modelling



Dry & humid isotherms

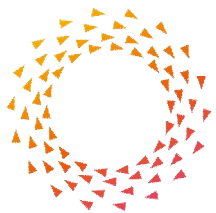
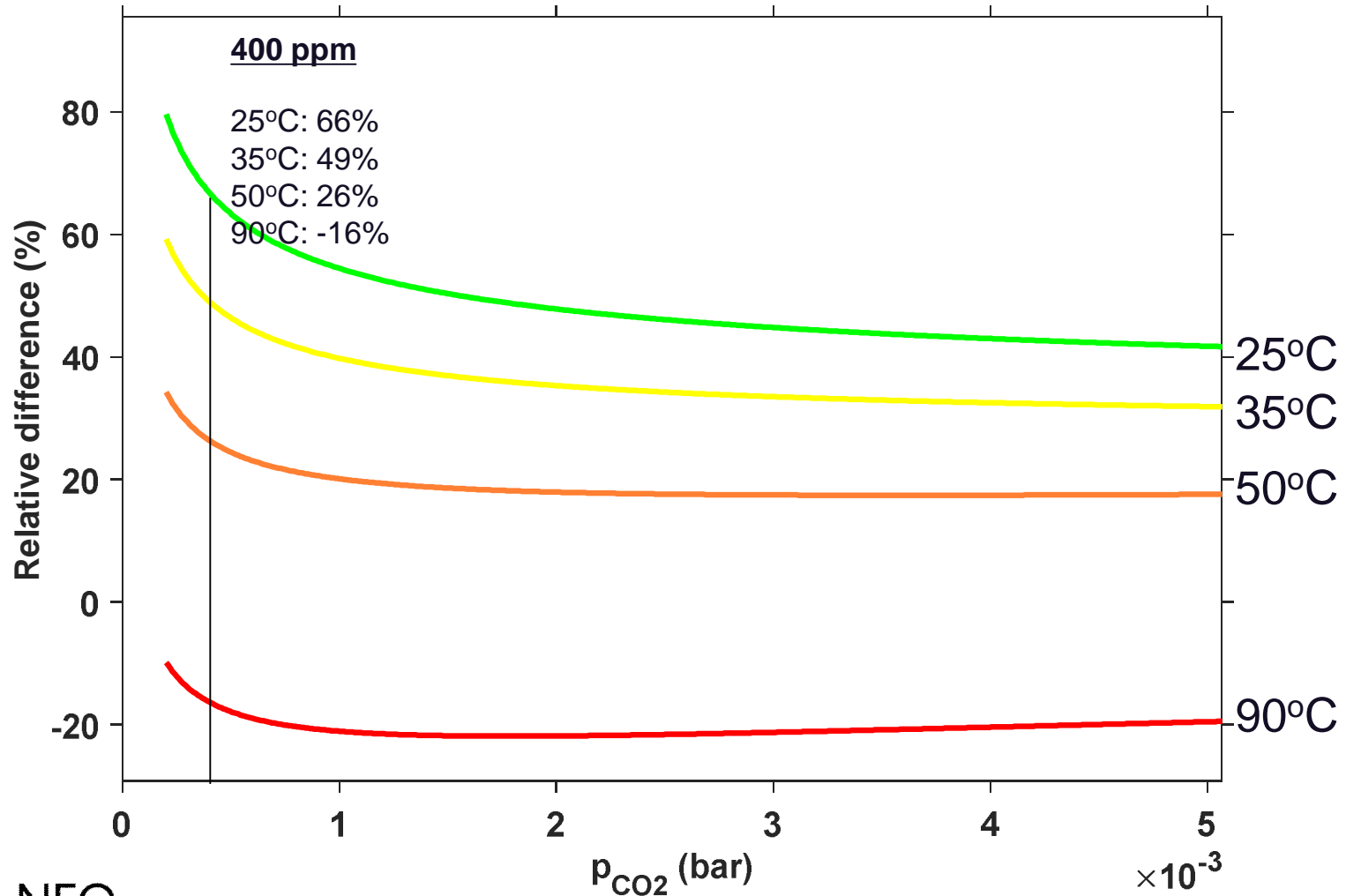


Lower capacity with humidity..?



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Dry capacity vs humid capacity

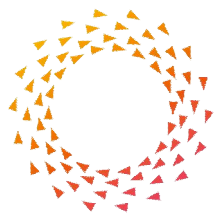
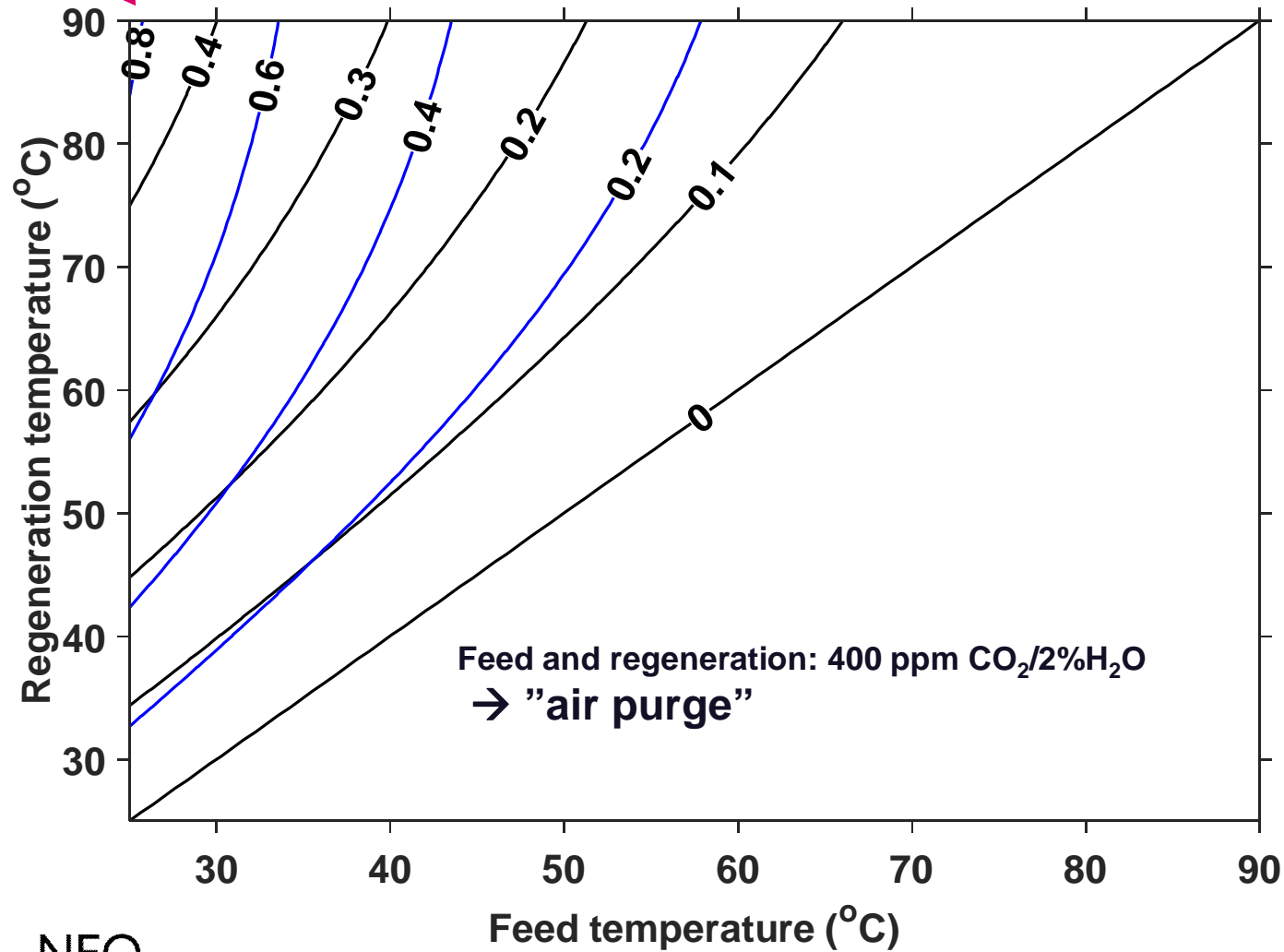


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- Strongest positive effect at the lowest temperature
- Negative (or no) effect at 90°C (close to boiling point)

Feed at room temperature, regeneration at 90°C:
 $EWC_{dry} = 0.45 \text{ mmol/g}$
 $EWC_{humid} = 0.82 \text{ mmol/g}$

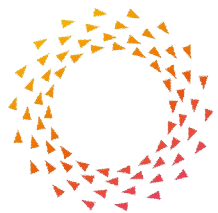
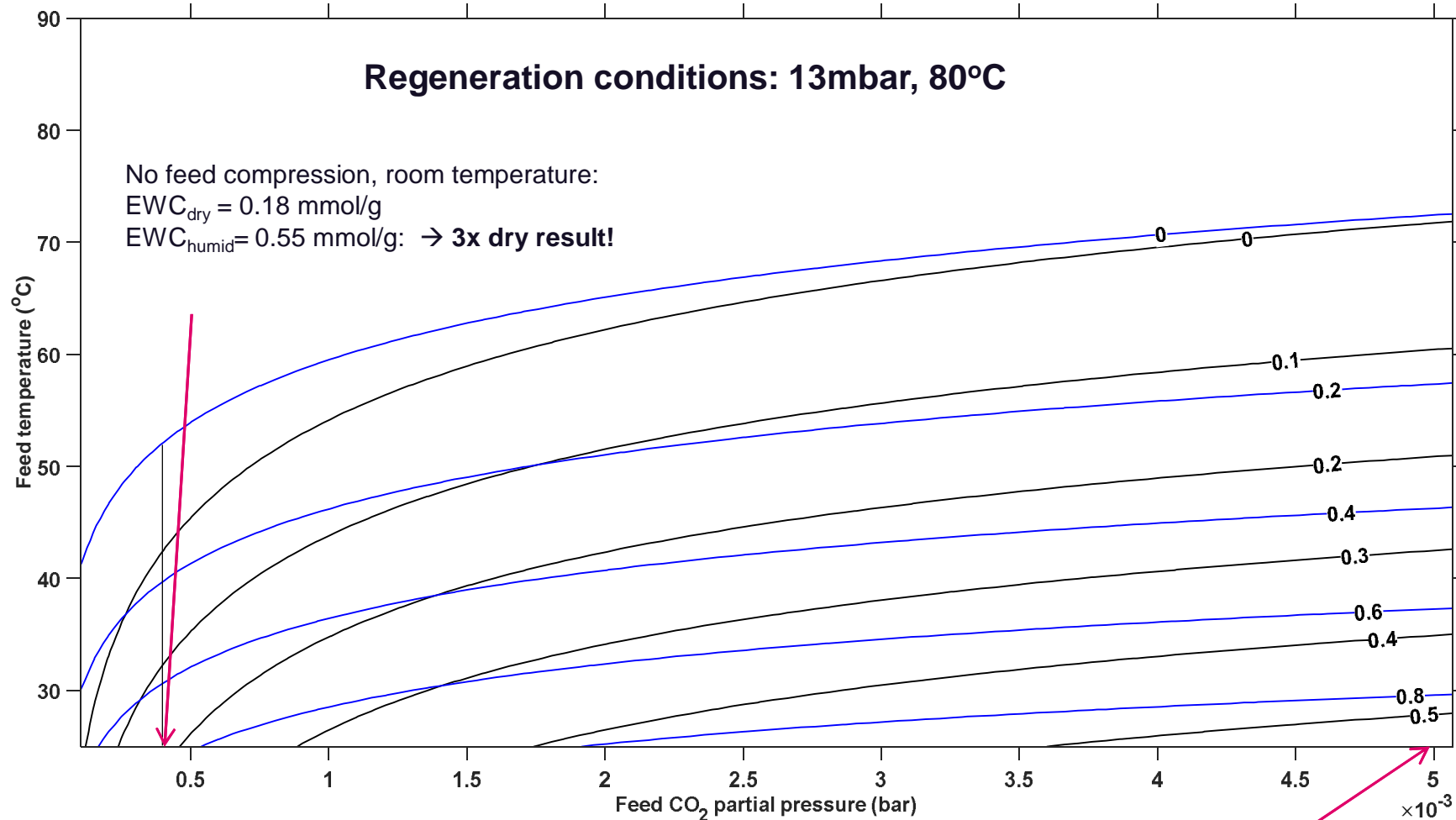
TSA working capacity



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- Humidity strongly promotes working capacity

TVSA working capacity

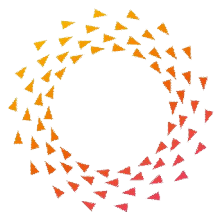


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Feed compression to 12,5 bar, room temperature:
 $EWC_{dry} = 0.54 \text{ mmol/g}$
 $EWC_{humid} = 0.93 \text{ mmol/g}$

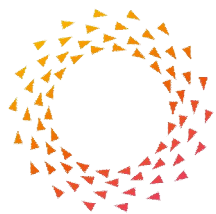
Water vs CO₂ adsorption

- Case: 400 ppm CO₂/2 vol-% H₂O
 - Adsorbed CO₂: 0.90 mmol/g
 - 66% increase compared to dry result
 - Adsorbed H₂O: 6.1 mmol/g
 - 6.8 mol of H₂O adsorbed / 1 mol CO₂
- Earlier case: 400 ppm CO₂/0.5 vol-% H₂O
 - Adsorbed CO₂: 0.70 mmol/g
 - 32% increase compared to dry result
 - Adsorbed H₂O: 1.6 mmol/g
 - 2.3 mol of H₂O adsorbed / 1 mol CO₂
- However, high amount of H₂O adsorption → high parasitic heat loss
 - finding optimum?



Conclusions & next steps

- Humidity strongly enhanced the CO₂ adsorption capacity
 - 66% at 25°C, 400ppm CO₂
- Also strong effect on working capacity, especially in TVSA for DAC without feed compression
- However, danger of high parasitic heat loss
 - Finding an optimum?
 - Possibility of pre-drying some amount?
- Important to model multi-component adsorption
 - H₂O isotherms required





NEO-CARBON Energy project is one of the Tekes strategic research openings and the project is carried out in cooperation with Technical Research Centre of Finland VTT Ltd, Lappeenranta University of Technology LUT and University of Turku, Finland Futures Research Centre FFRC.

Isotherms with experimental points

