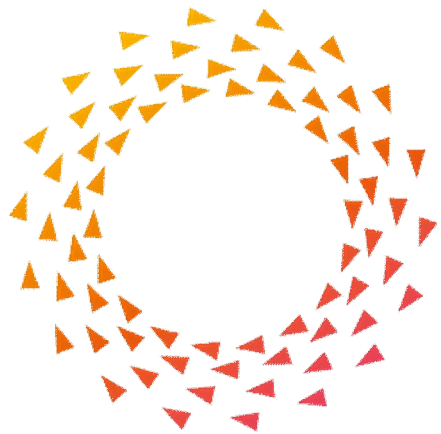




Effect of impurities on hydrogenation of CO₂ Master's thesis



**NEO
CARBON
ENERGY**

Fanny Henriksson
Neo-Carbon Energy seminar
30.8.2016

Structure

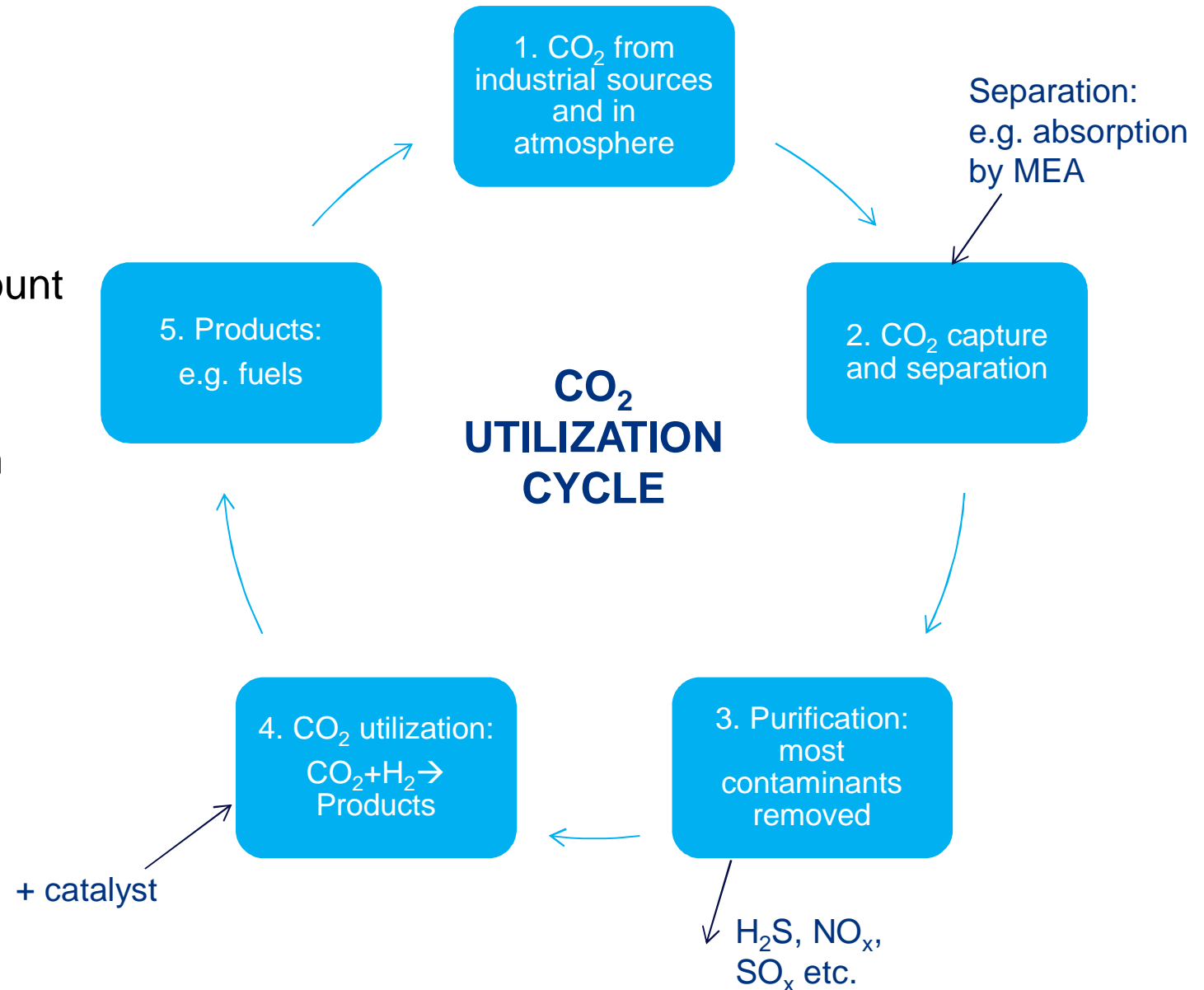
- Motivation and aim
- Experimental part
- Results

Motivation and aim

Motivation

- Reduce CO₂ emissions

- 1) decrease amount of CO₂ produced
- 2) CO₂ storage
- 3) CO₂ utilization



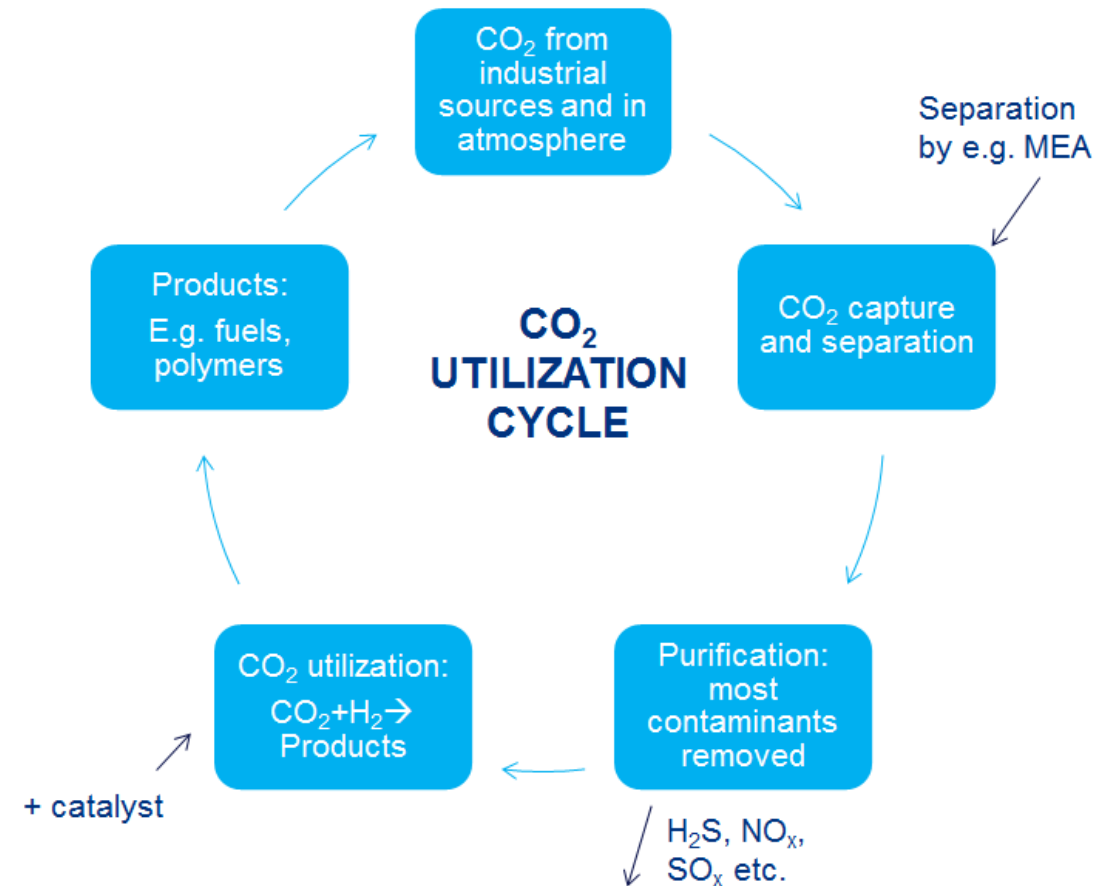
Aim

Aim:

- Find out how impurities in separated CO₂ affect CO₂ hydrogenation and catalyst used

Special emphasis:

- Effect of MEA and H₂S on product formation
- MEA was selected due to lack of earlier studies
- H₂S was selected since it is a typical catalyst poison, common impurity and due to contradictory in earlier studies



CO₂ hydrogenation reactions and catalysts

1.	CO + H ₂ O	RWGS
2.	CO + 2 H ₂ → (CH ₂) _n + H ₂ O	Fischer-Tropsch synthesis
3.	CO ₂ + 4H ₂ → CH ₄ + 2H ₂ O	Methanation
4.	CO ₂ + 3H ₂ → CH ₃ OH + H ₂ O	Methanol synthesis

- Different catalysts favour different reactions
- Cu-based: Methanol synthesis & RWGS
- Ni-based: Methanation
- Fe-based: RWGS & FT synthesis

Experimental part

Experiments

- Temperature programmed desorption (TPD) experiments
 - Effect of MEA studied
 - Gas analyzed by MS
 - Catalyst characterization and formation of CH₄ studied
- Reaction tests in a plug flow reactor(PFR)
 - Effect of H₂S studied
 - Gas analyzed by GC
 - Detailed information about type and amount of product formed

Both experiments focus on $\text{CO}_2 + \text{H}_2 \rightarrow \text{products}$

TPD experiments

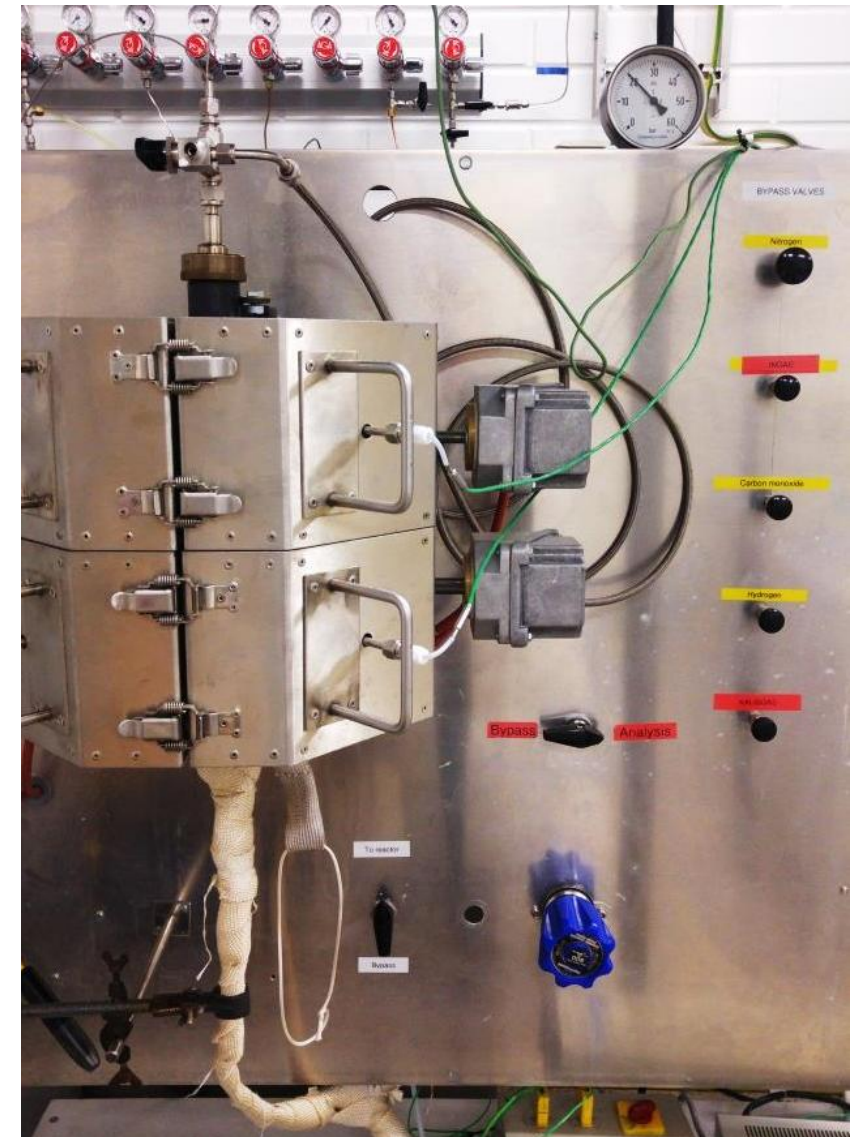


Reaction tests in 300 °C in atmospheric pressure:

- Effect of MEA studied
 - MEA (573 ppm) connected to carrier gas
- Formation of CH₄ followed
- Constant H₂ flow, to which CO₂ is pulsed

Reaction tests in PFR

- Effect of H₂S studied
- Pre-mixed reactant gas → continuous reaction
- Five phases for each catalyst
 1. Initial reaction
 2. 1st poisoning
 3. 1st recovery
 4. 2nd poisoning
 5. 2nd recovery



Catalysts

- Four different catalysts studied
 - 2xFe-based → FT products
 - Cu: → CH₃OH
 - Ni: → CH₄

Name	Components	Pellet size (mm)	Density (g/cm ³)	BET surface area (m ² /g)	Producer	Experiments
FeMn	5Fe:5Mn:Al ₂ O ₃	~7x1.2	0.42	200	in-house	TPD & PFR
low α -Fe	100Fe:4.6Si:2Cu:1.4K	pulverized	Unknown	Unknown	in-house	TPD & PFR
Cu	Unknown*	1.5x1.5	1.8	64.8	BASF	TPD & PFR
Ni	Unknown**	0.2-0.3	Unknown	Unknown	BASF	TPD

* CuO: 50<wt%<75, ZnO 15<wt%<20

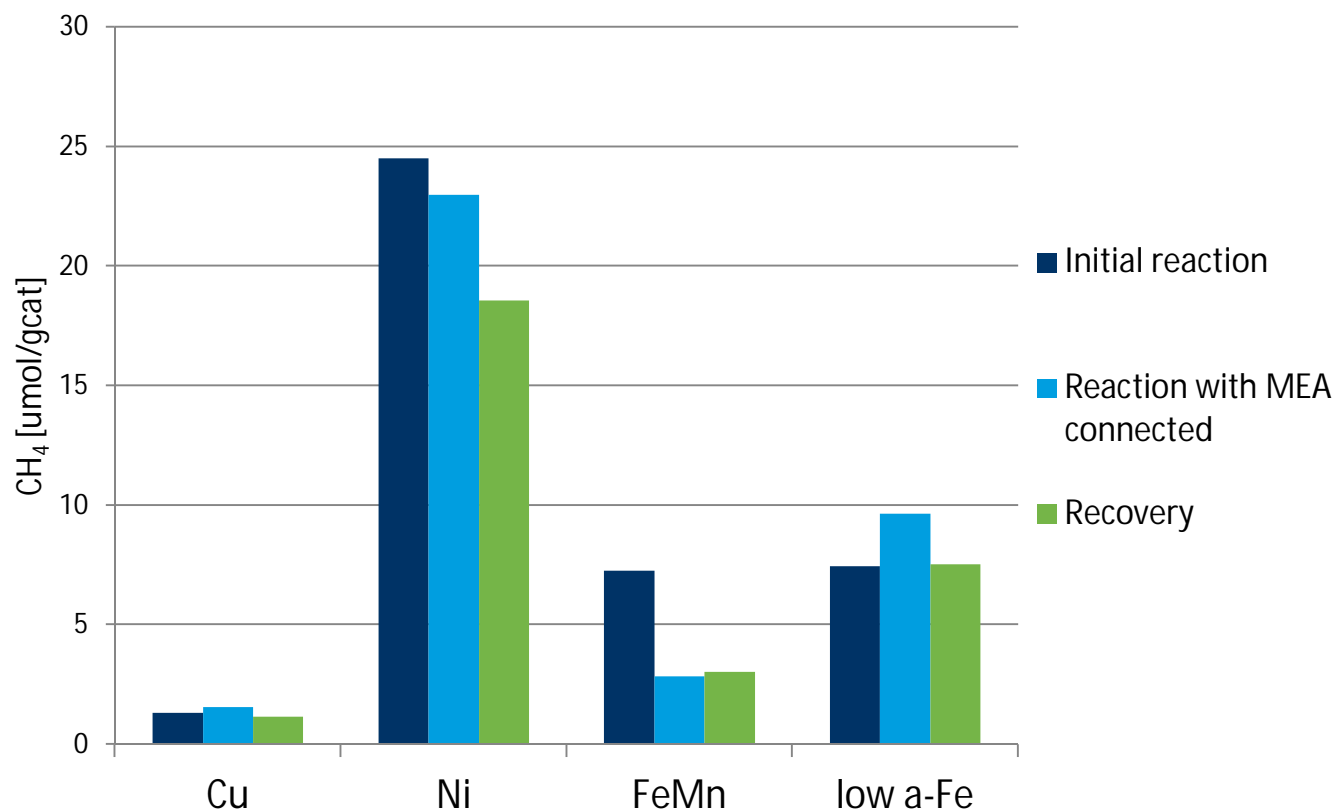
**NiO: 15 wt%

Results

TPD – Effect of MEA

- MEA has an
 - increasing effect on CH_4 formation for Cu and low α -Fe catalysts
 - decreasing effect on CH_4 formation for Ni and FeMn catalysts, from which the catalyst does not recover

Effect of MEA on CH_4 formation



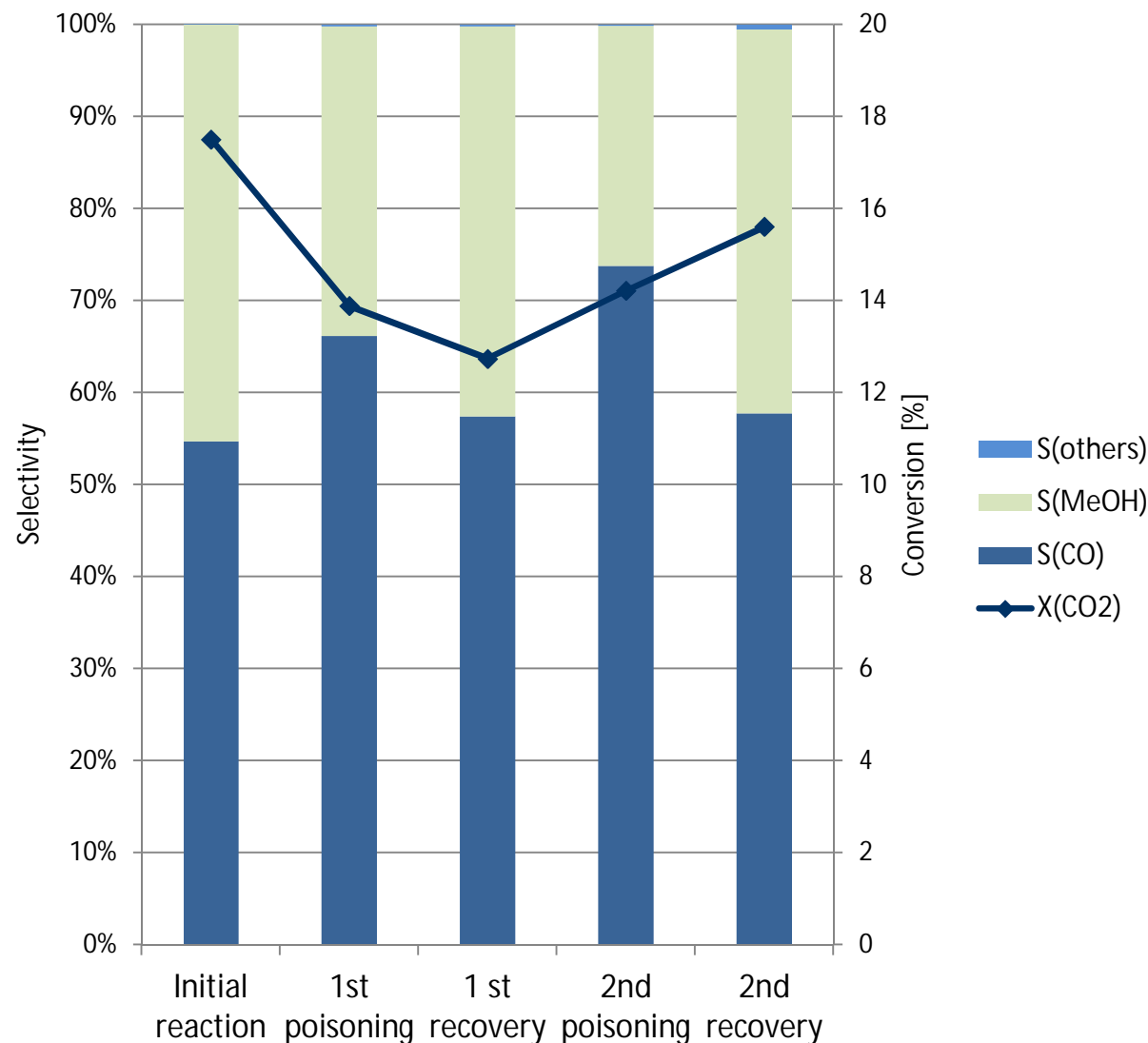
Reaction tests – Effect of H₂S on Cu catalyst

Cu: Conversion and selectivity at T=230 °C and p=30 bar

- 1st poisoning: 33.2 ppm
- 2nd poisoning: 60 ppm

- Conversion drops slightly, but recovers
- Methanol selectivity decreases during poisoning

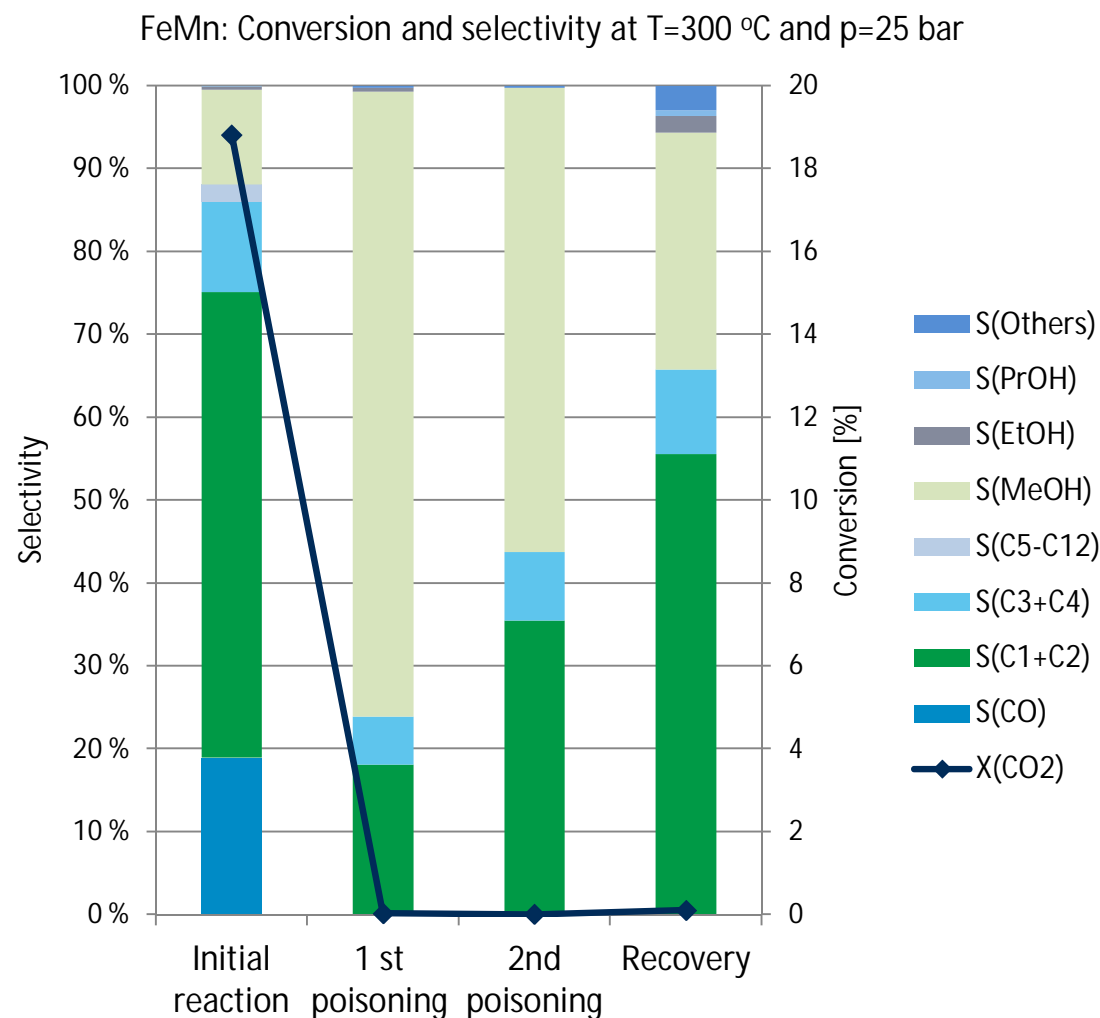
- Surprisingly good resistance against H₂S
- Selectivity change due to:
 - RWGS being more spontaneous than the methanol synthesis
 - lower WHSV during poisoning → decomposition of methanol to CO



Reaction tests – Effect of H₂S on FeMn catalyst

- 1st poisoning: 33.2 ppm
- 2nd poisoning: 59.8 ppm
- Catalyst deactivates at 1st poisoning
- Catalyst does not recover

→ Sensitive to H₂S poisoning

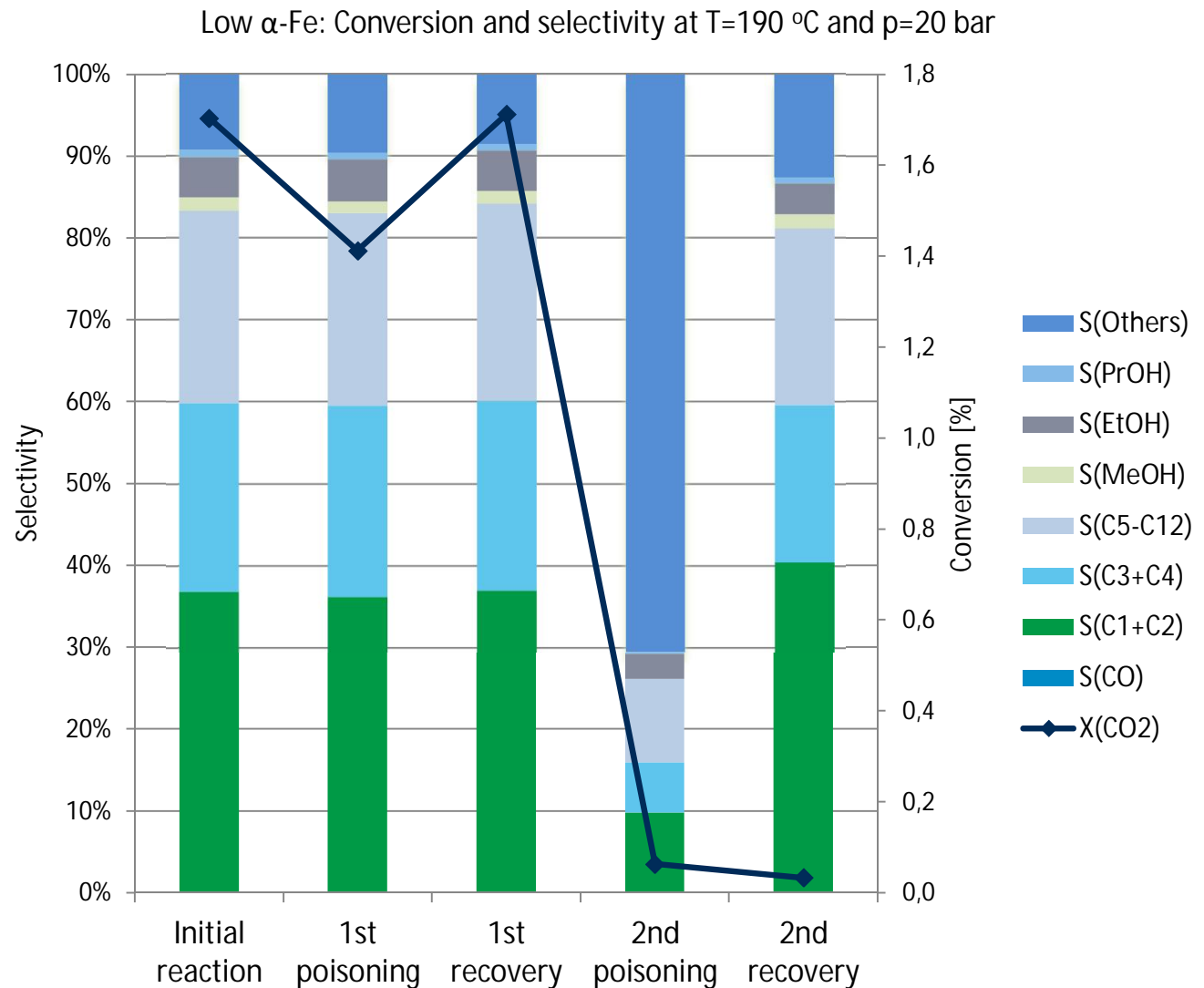


Reaction tests – Effect of H₂S on low α -Fe catalyst

- 1st poisoning: 1.1 ppm
- 2nd poisoning: 63.2 ppm

- Catalyst deactivates during 2nd poisoning and does not recover
- Selectivities remain unaffected

- Some (or most) sites deactivate completely, while others remain unaffected



Conclusion

Effect of MEA

- Cu & low α -Fe catalysts improved their formation of CH_4
 - Negative effect on other catalysts
- Future studies should focus on studying selectivities in detail to confirm whether MEA actually has an increasing effect on CH_4 formation

Effect of H_2S

- Cu catalyst: Surprisingly resistant to H_2S , but selectivity was modified
 - Fe-based catalysts: Deactivated and did not recover
- The effect of lower concentrations of H_2S could be studied for Fe-based catalysts

References

Arena, F., Mezzatesta, G., Spadaro, L. & Trunfio, G., 2014. Latest advances in the catalytic hydrogenation of carbon dioxide to methanol/dimethylether. In *Transformation and Utilization of Carbon Dioxide*. pp. 103–130.

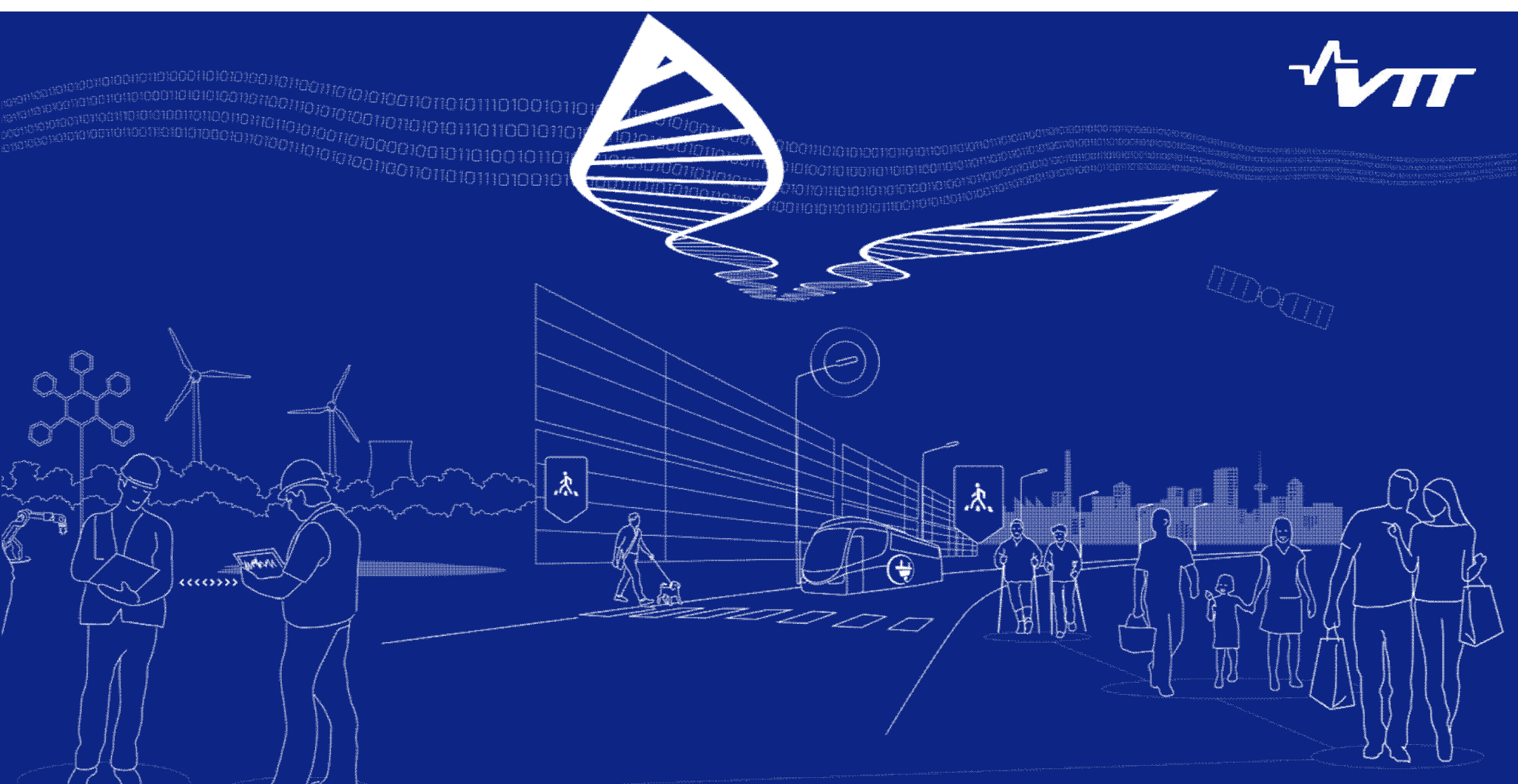
Ma, W., Jacobs, G., Sparks, D.E., Shafer, W.D., Hamdeh, H.H., Hopps, S.D., Pendyala, V.R.R., Hu, Y., Xiao, Q. & Davis, B.H., 2015. Effect of ammonia in Syngas on the Fischer-Tropsch Synthesis Performance of a Precipitated Iron Catalyst. *Applied Catalysis A: General*, (326), pp.149–160.

Ma, W., Jacobs, G., Sparks, D.E., Thomas, G.A., Shafer, W.D., Sparks, D.E., Pendyala, V.R.R., Hopps, S.G., MacLennan, A., Hamdeh, H.H., Hu, Y. & Davis, B.H., 2015. Effect of H₂S in syngas on the Fischer-Tropsch synthesis performance of a precipitated iron catalyst. *Journal of Catalysis*, 326, pp.149–160.

Sexton, A.J. & Rochelle, G.T., 2011. Reaction products from the oxidative degradation of monoethanolamine. *Industrial and Engineering Chemistry Research*, 50(2), pp.667–673.

Wang, W., Wang, S., Ma, X. & Gong, J., 2011. Recent advances in catalytic hydrogenation of carbon dioxide. *Chemical Society reviews*, 40(7), pp.3703–27.

Yoshihara, J. & Campbell, C.T., 1996. Methanol Synthesis and Reverse Water–Gas Shift Kinetics over Cu(110) Model Catalysts: Structural Sensitivity. *Journal of Catalysis*, 161(2), pp.776–782.



**Thank you for your attention!
Any questions?**