

H₂-BASED IRONMAKING

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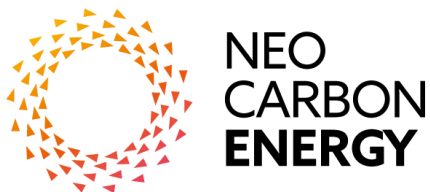
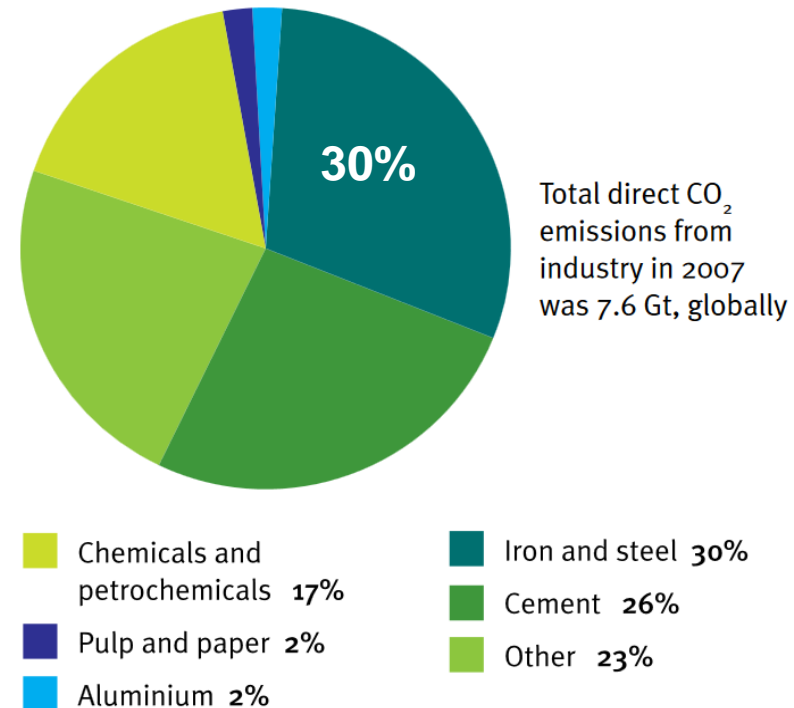


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Researcher's Seminar
August 23rd-24th 2017, Lappeenranta

Background & scope

- Iron&steel sector is a marked contributor to CO₂ emissions from industry
- VTT has studied options for significant emissions reductions in iron&steel industry in several projects and developed a feasibility evaluation tool
- One important alternative was missing: Iron ore can be reduced with H₂ enabling virtually CO₂-free iron/steel

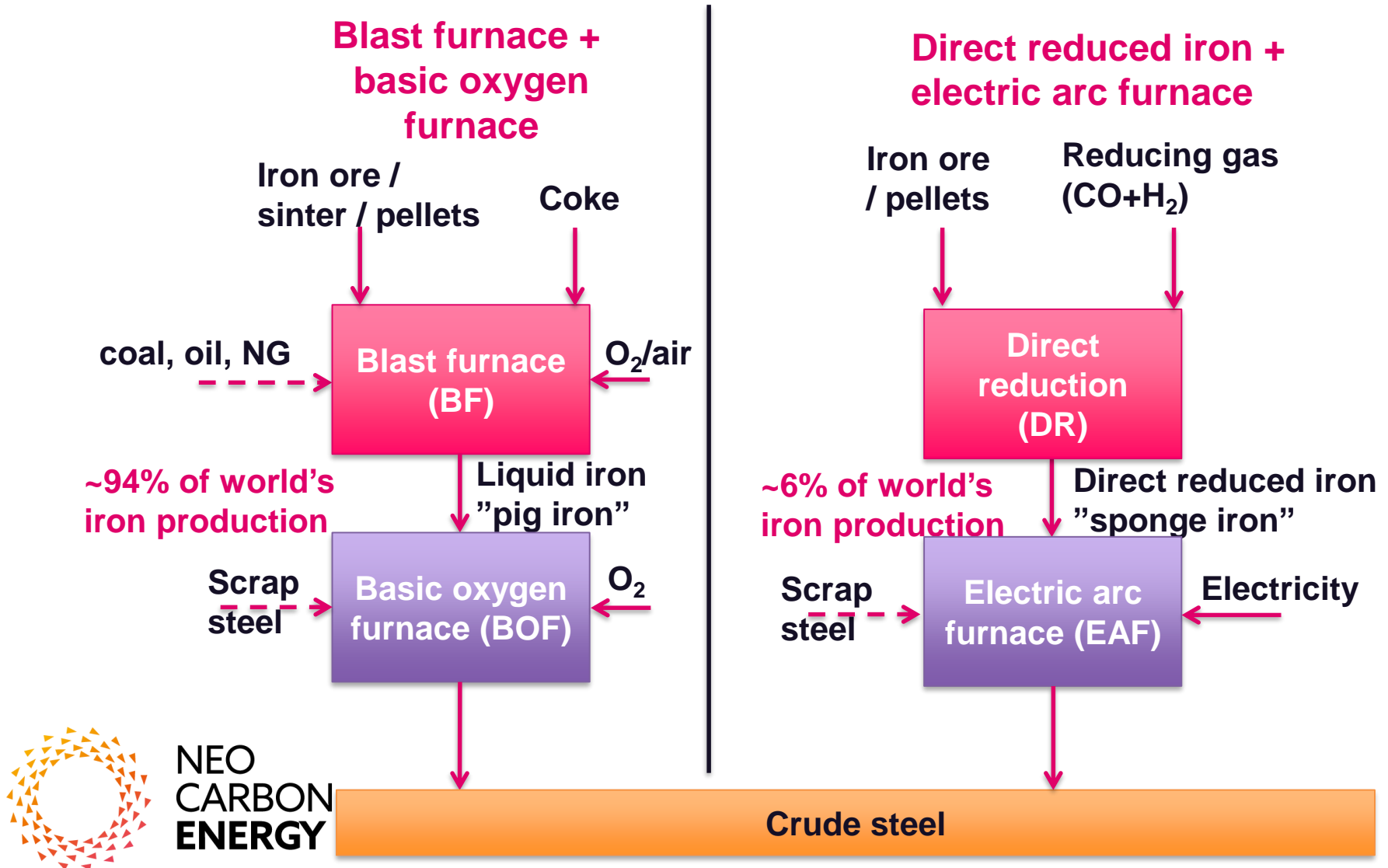


Data: IEA Energy technology perspectives 2010
 Fig: [Reducing CO2 emissions from heavy industry 2012](#)



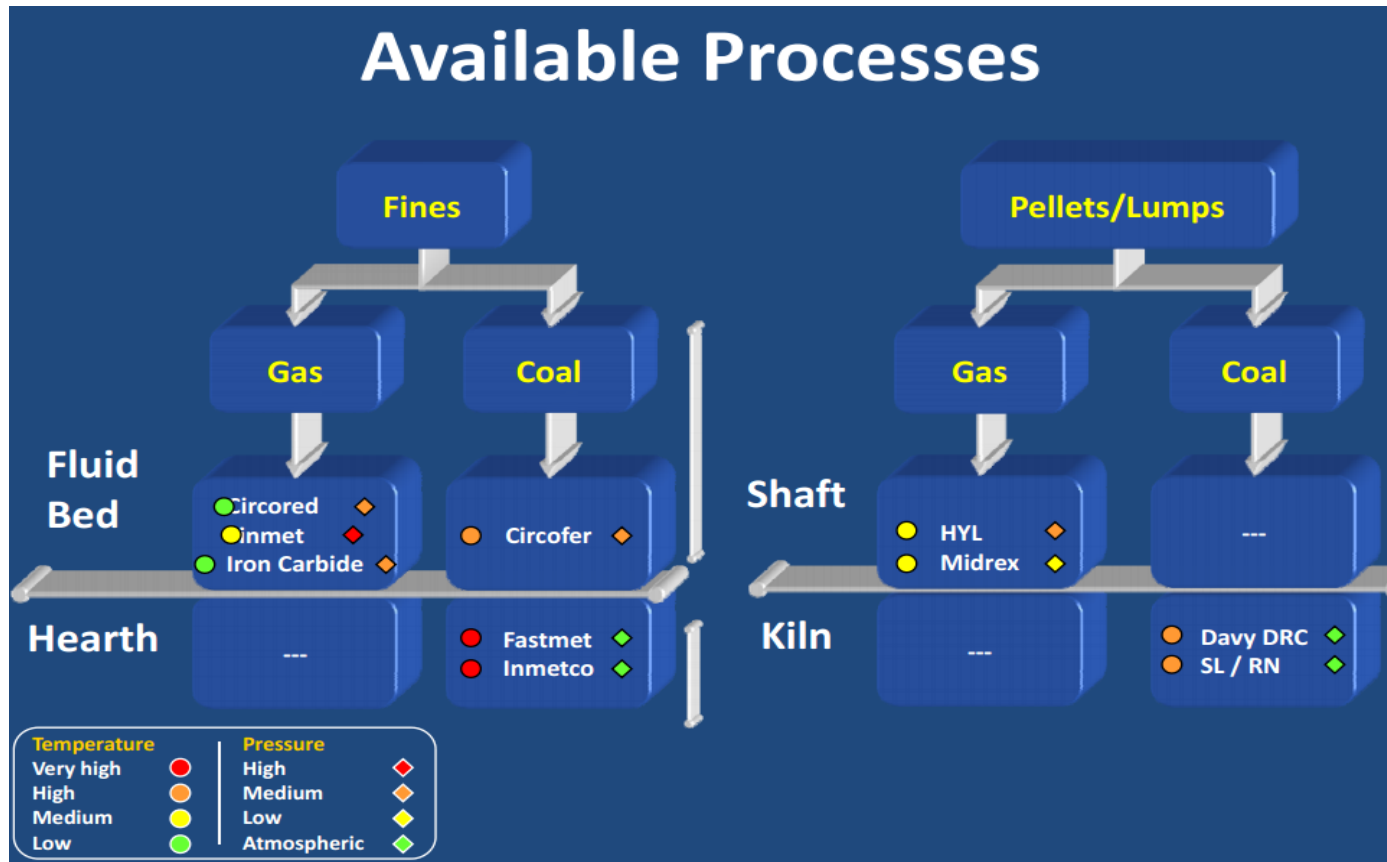
STEEL PRODUCTION

Primary(=ore-based) steel production



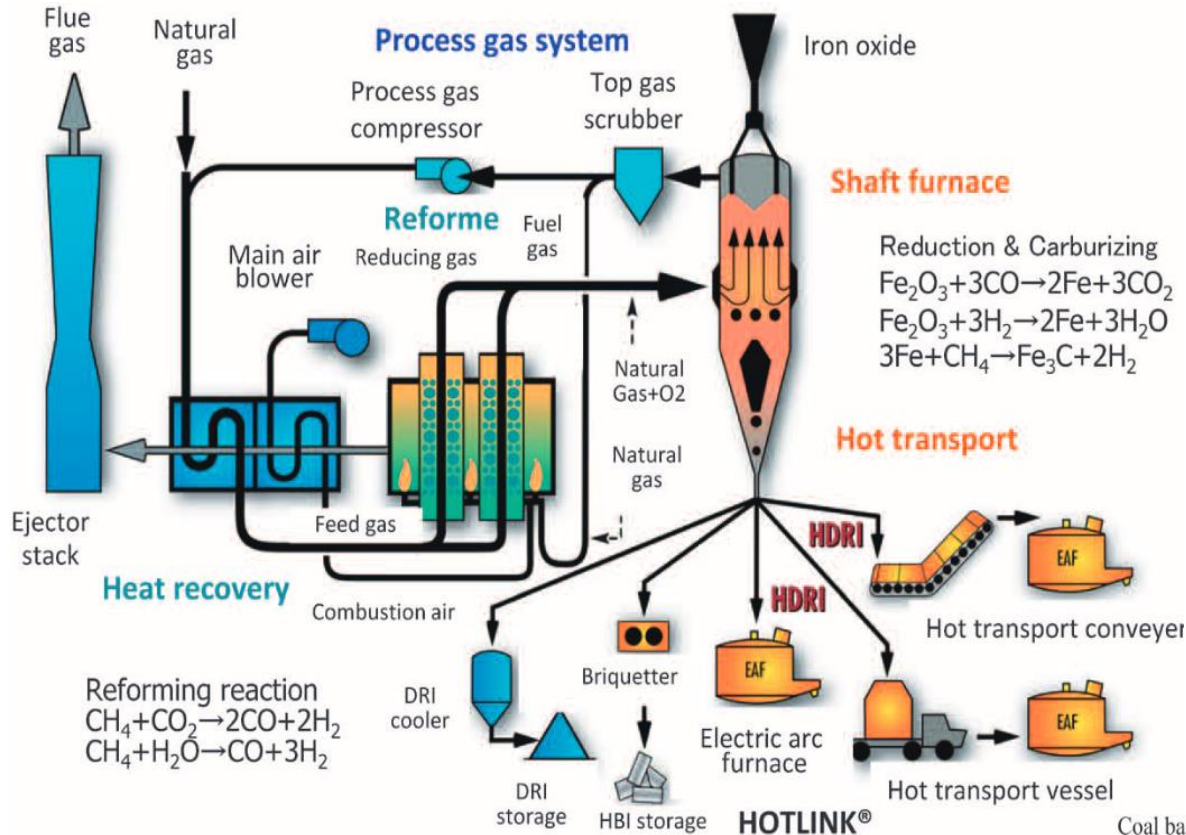
Direct reduced iron

Various process alternatives



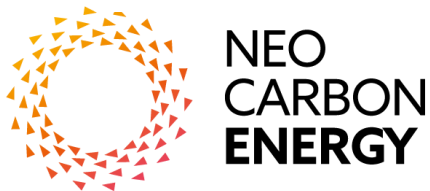
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MIDREX – The most common DRI process



Reducing takes place in solid state (~800-1050° C)

Fig. 7 MIDREX process flow sheet⁸⁾



Tanaka (2015). Resources Trend and Use of Direct Reduced Iron in Steelmaking Process

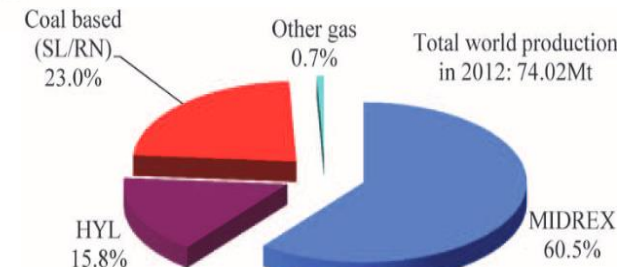


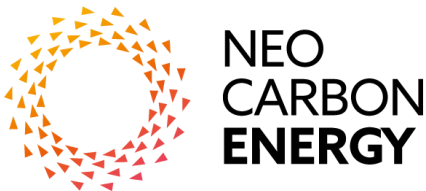
Fig. 6 World DRI production processes in 2012⁵⁾



DRI USING HYDROGEN?

Direct reduced iron with pure H₂

- Hydrogen would be a good reducing agent:
 - H₂ has been shown to react more rapidly than CO → reactor size can be decreased compared to current MIDREX and HYL [1]
-but price and availability are a challenge
- Using pure H₂ is more or less in development phase still
 - Few different processes/approaches
 - Circored (Outotec's dual fluid bed process, H₂ from natural gas, "commercial")
 - Hydrogen Flash Ironmaking (University of Utah, fundamental research [2])
 - **H₂ in shaft kiln ("H₂ Midrex")**



[1] da Costa et al (2014). Modelling a new low CO₂ emissions hydrogen steelmaking process

[2] Sohn&Mosabbad (2016). Development of a Novel Flash Ironmaking Technology with Greatly Reduced Energy Consumption and CO₂ Emissions



H₂ DRI

**THEORETICAL CASE STUDY BASED ON
LITERATURE SOURCES**

Case description

- **H₂ DRI case:** investment into an electrolytic H₂-based direct reduced iron process
- **Vs**
- **Reference case:** refurbishment of the current process
- Mill capacity ~2.6 Mt_{crude steel/a}

Changes in:

- Electricity consumption
- Direct CO₂ emissions
- Coke and PCI coal consumption
- LNG purchase
- O₂ purchase/sales
- CAPEX



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H₂ DRI case

- Electrolysers + shaft furnace H₂ direct reduction process + electric arc furnace (EAF)
- Storage of hydrogen is not considered (electrolysers assumed to be run 8600 h/a at full capacity)
- Coke gas assumed to be replaced by additional LNG in steel rolling processes and a small amount of coal is still used in the electric arc furnace
- No change in district/process heat revenues (large excess) or other OPEX

Electricity requirement for electrolytic H₂ DRI process

	GJ/t crude steel
Hydrogen/electrolysis	11.5
DRI	0.439
EAF	2.068
Hot rolling	0.375
SUM	14.3

Values based on Fishedick et al. / Journal of Cleaner Production 84 (2014) 563-580, adjusted to suit to studied case, for example the lower scrap metal content



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CAPEX

	Reference case	H ₂ DRI case
Blast furnace refurb.	74 €/t CS [2]	
Basic oxygen furnace refurbishment	64 €/t CS [2]	
Coke plant refurb.	17 €/t CS [2]	
TOTAL	=155 €/t crude steel	
DRI process		161* €/t CS [2]
Electric arc furnace		184 €/t CS [2]
Electrolysers		650 €/kW _{LHV} [1] 236 €/t CS
TOTAL		=581 €/t crude steel

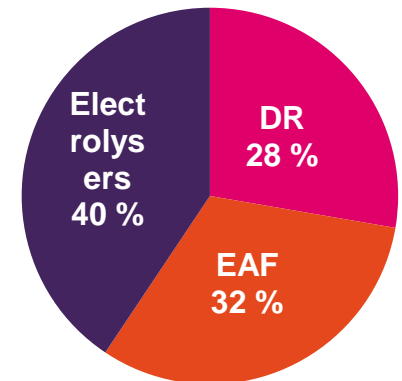
[1] Fishedick et al. / Journal of Cleaner Production 84 (2014)

[2] Wörtler et al. (2013). Steel's Contribution to a low Carbon Europe 2050.

*process using electrolytic H₂ was assumed to cost 30% less than natural gas based MIDREX



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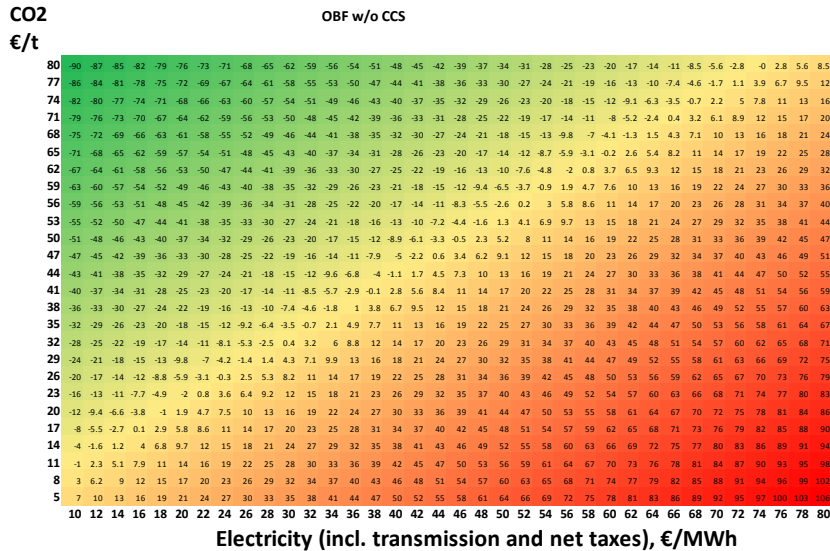


Implications of adopting H₂ DRI

- Direct **CO₂ emissions** would be **reduced by almost 90%**
- **Electricity consumption** would **increase more than 10 TWh**
- **~1 TWh more LNG** would be required for rolling
- **Over 1 Mt of oxygen** would be produced as a by-product
 - total demand in Finland is ~1.3 Mt/a.

Economics?

Excel tool



- Profitability maps vs. reference case are shown for the studied case
- Sliders for sensitivity analysis



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LNG price	<input type="text" value="40"/>	40 €/MWh
Coal price (PCI)	<input type="text" value="12"/>	12 €/MWh
Coke price/value	<input type="text" value="150"/>	150 €/t
Biocoke price	<input type="text" value="40"/>	40 €/MWh
C-neutral MeOH value	<input type="text" value="76"/>	76 €/MWh
WACC	<input type="text" value="11"/>	11%
Economic timeframe	<input type="text" value="16"/>	16 years
Investment sensitivity	<input type="text" value="4"/>	4%
CO2 trans.&storage cost	<input type="text" value="40"/>	40 €/t
HKA	<input type="text" value="8600"/>	8600 h/a
Share of biocoke	<input type="text" value="50"/>	50% of PCI (enb.)
Value of oxygen	<input type="text" value="70"/>	70 €/t
Value of surplus oxygen	<input type="text" value="2"/>	2 €/t

Default market prices/values

	Value	Unit
LNG	42	€/MWh
Coal (for PCI or EAF)	12	€/MWh
Coke	150	€/t
Value of excess oxygen	10*	€/t

*low average price as it is not reasonable to assume that all of the oxygen could be sold

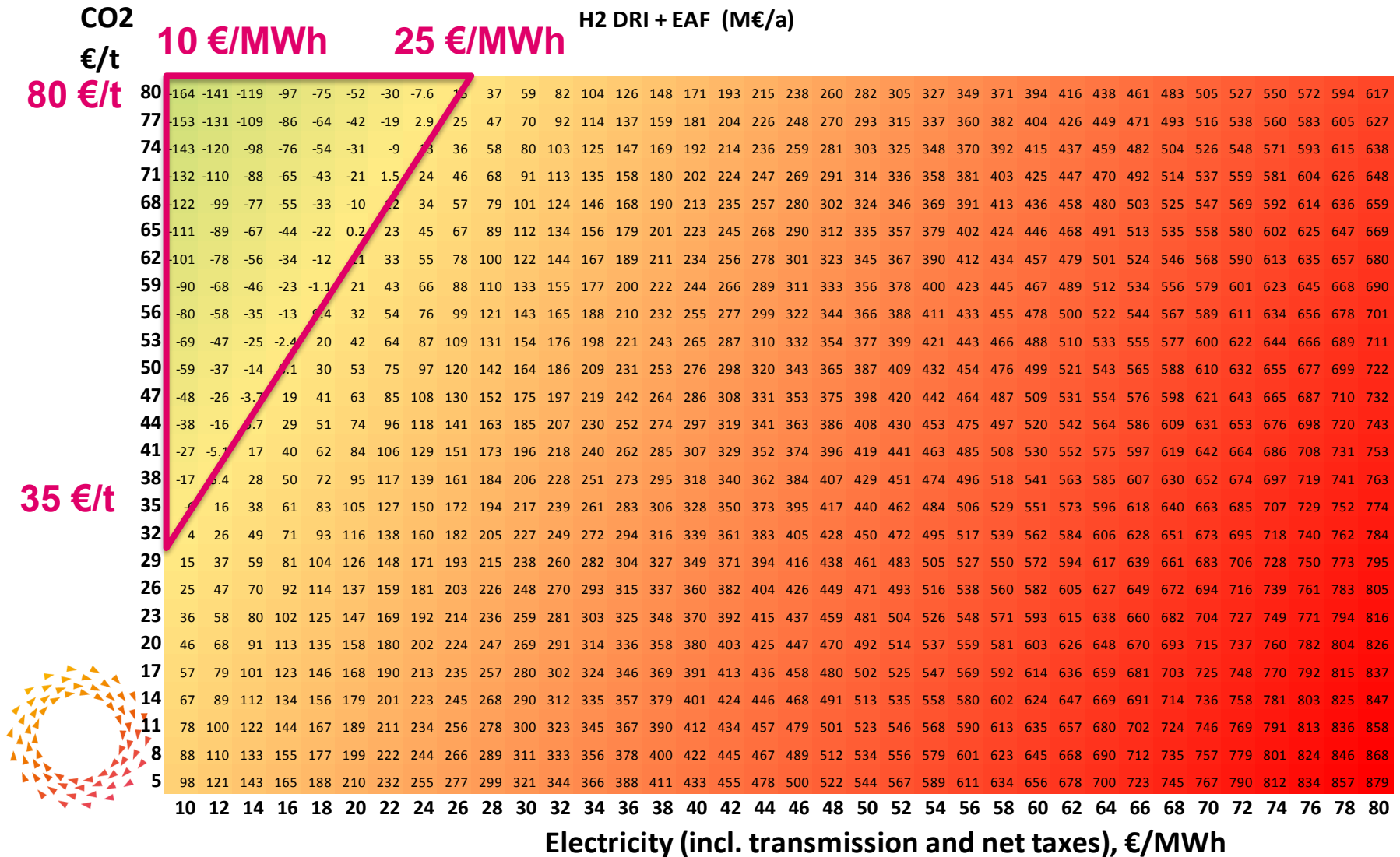


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WACC 8%, timeframe 20 years

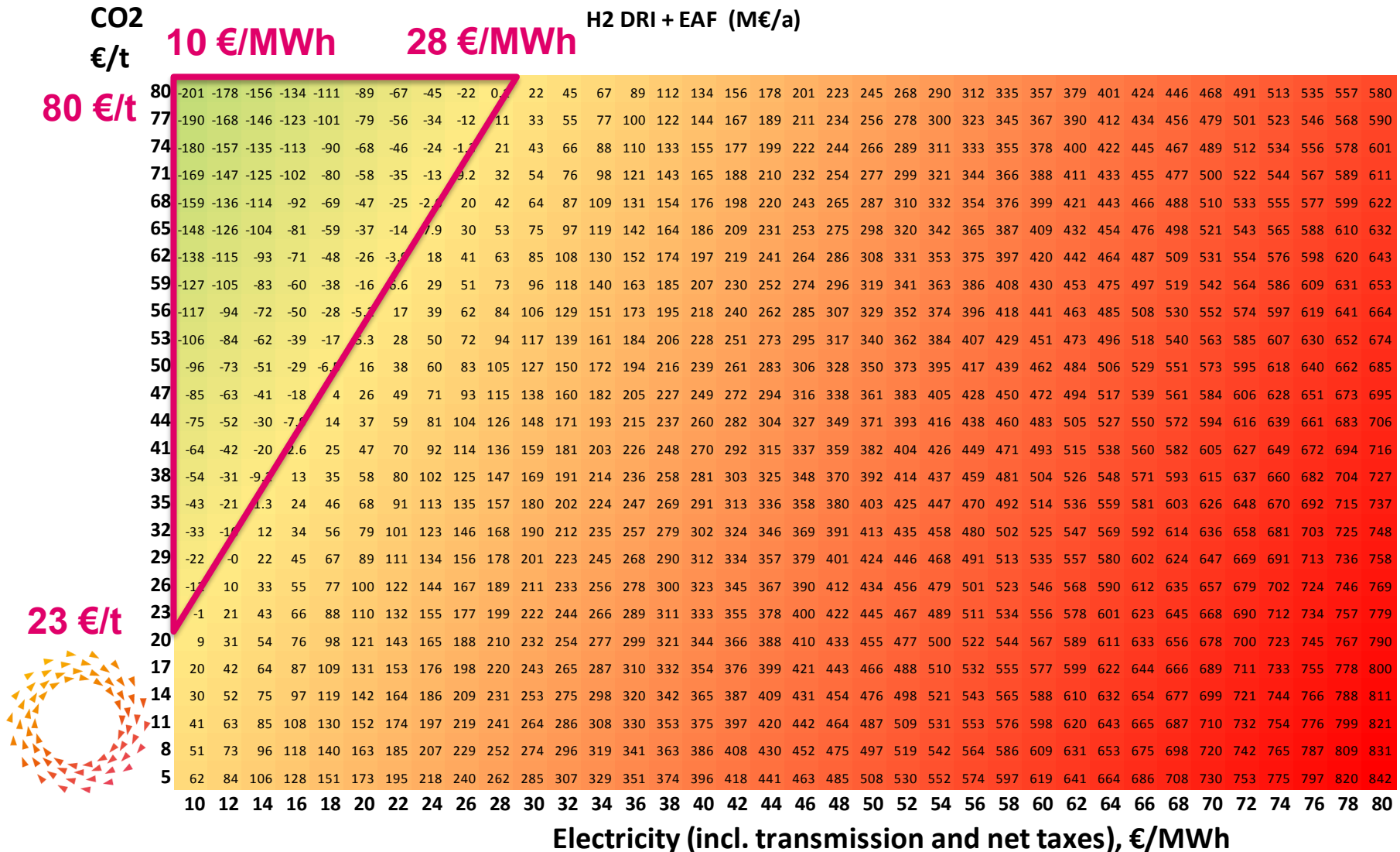
Additional cost (M€/a) compared to reference case

Default values



Additional cost (M€/a) compared to reference case

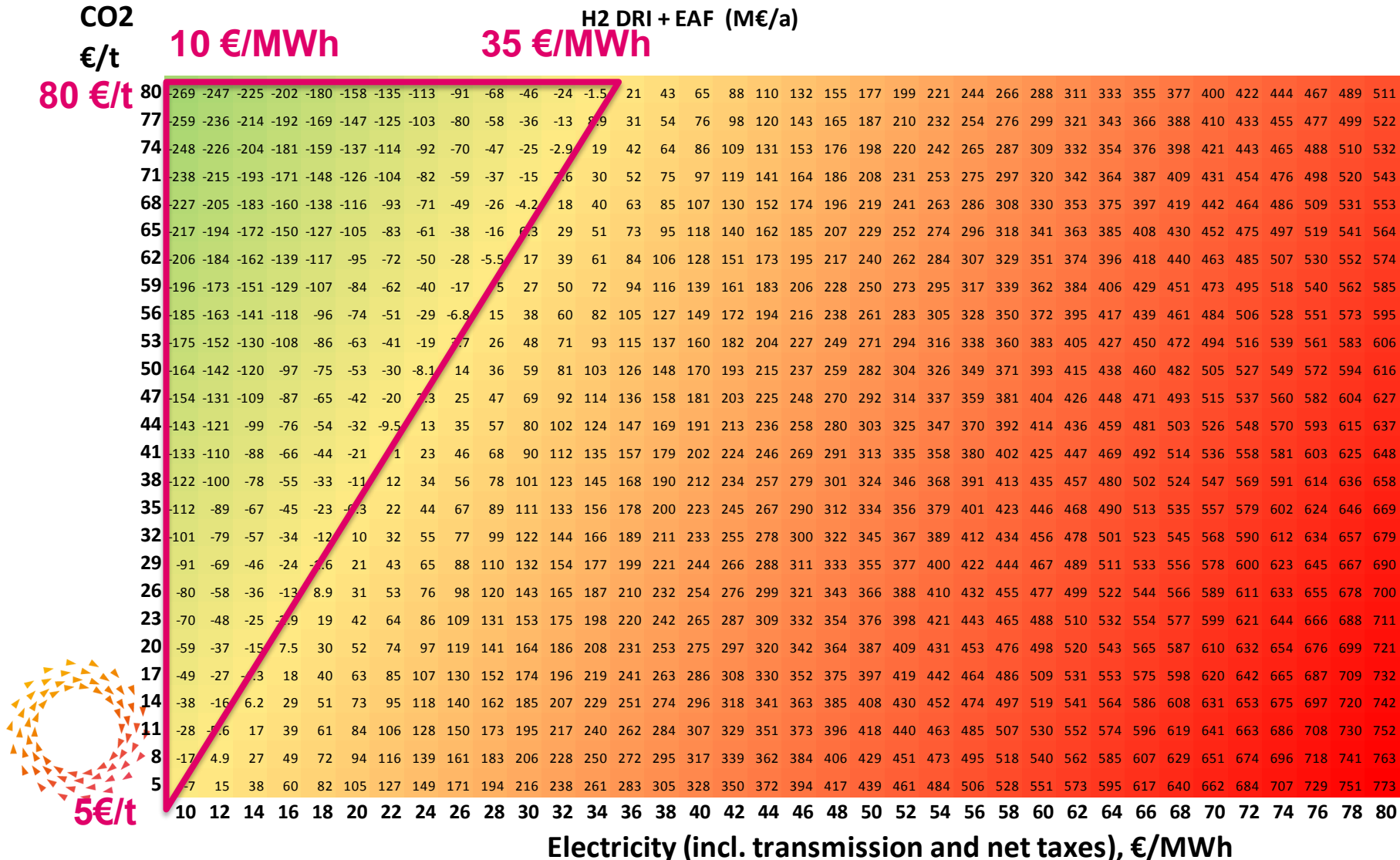
Electrolyser CAPEX 650→300 €/kW





Additional cost (M€/a) compared to reference case

Electrolyser CAPEX 650→300 €/kW & Greenfield BF+BOF



Conclusions & next steps

- DRI w/ electrolytic H₂ could enable basically CO₂-free steel production
- Process seems technically feasible but economics seem a bit challenging
 - But as CCS still faces a lot of opposition and obstacles, H₂ route might still be the way to go



THANKS!